

Investigation of Applying NF Membrane for Dye Removal Using Multivariate Regression Model

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Abstract : Recently, Nanofiltration plays an important role in dye wastewater treatment. The efficiency of membrane separation system for wastewater treatment plant is complicated due to different operating conditions involved in the separation process. Estimation of the Nanofiltration membrane performance is essential to evaluate the final water quality for further reuse. This work focus on the development of a simplified predictive model for membrane performance estimation under a set of parameters. A linear multiple regression model with coefficient of determination (R^2) of 1 has been developed for COD values in the permeate stream, while (R^2) of 0.85 for membrane rejection estimation. Seven investigated parameters have been related to formulate the model. The model has been applied for dye wastewater scheme comprising Nanofiltration with proper pretreatment. The model has been validated with an average deviation of 15% for membrane rejection and almost no deviation for COD level estimation in the permeate stream.

Keywords : Nanofiltration, Membrane separation, Wastewater Treatment, predictive model, Reactive dye.

1. Introduction

Textile dyeing industry is one of the largest water consuming industries. The effluent wastewater produced from the dyeing industries contains different chemicals and coloring agents and hence this effluent requires proper treatment before its discharge (Do and Chem¹). The dye house effluents are difficult to be treated because of the variable composition in the waste stream (Najmeh et al. ²). In addition to color, the textile wastewater the characteristics of high pH, high COD and low biodegradability (Mohammed³). Textile wastewater has a dramatic environmental impact and cannot be directly discharged to a receiving water body (Marrot & Roche ⁴); therefore, textile wastewater treatment is mandatory due to the high water consumption rate and the environmental impacts (Chaia-Hung et al. ⁵).

The major sources of color in textile effluents are the dyes from the dyeing operations. There are three groups of textile dyes dependent on their state in solution as well as their charge: group N; neutral dyes such as disperse, vat and Sulphur dyes which are insoluble in water; group C; cationic dyes like basic dyes and group A; anionic dyes that is to acid, direct and reactive dyes which are soluble in water (Ahmad et al. ⁶). Furthermore, as a result of low biodegradability of most of the dye groups used in textile industry, biological treatment by activated sludge is not always effective due to aerobic biological treatment and oxidizing agent's resistance (Jiratananon et al. ⁷). An advanced treatment technique is required, especially if the treated wastewater will be recycled/reused (Kapadan & Kargi ⁸). Membrane separation is an optimal solution to remove color, COD and salinity (Aouni et al. ⁹).

Nanofiltration (NF), is a newly developed membrane technology for various water treatment and purification purposes (Koyuncu *et al.*¹⁰); (Valentina *et al.*¹¹). Although, membrane processes require proper pretreatment techniques, many approaches have been studied to minimize membrane fouling and reduce the costs (Koyuncu *et al.*¹²). Pretreatment of feed water includes optimization of operating conditions such as pH as well as chemicals consumption and recovery ratio (Hong & Elinlech¹³; Koyuncu *et al.*¹⁴). Microfiltration (MF) and ultrafiltration (UF) can be used as a pretreatment step for Nanofiltration (Gozalvez-Zafrilla *et al.*¹⁵; Debik *et al.*¹⁶; Ong *et al.*¹⁷; Barredo-Damas *et al.*¹⁸; Alventosa-delara *et al.*¹⁹).

Many studies have been carried out on color removal from textile wastewater by Nanofiltration processes. Lebrun *et al.*, investigated electric field enhanced Nanofiltration process by BQ01 and NF45 membranes in dye removal. The results showed variations in dynamic permeability in the presence of electrolytes and according to the electrical potential applied (Lebrun *et al.*²⁰). Fuchs *et al.*, studied membrane bioreactor (MBR) performance in textile wastewater treatment, and explored its ability to achieve water quality meeting reuse criteria. COD removal was found to vary between 60 and 95 % and COD levels reduced at lower volumetric loading rates that was tested (Fuchs *et al.*²¹). Das Gupta *et al.*, studied Nanofiltration with MWCO = 400 Dalton to treat the effluent from a textile plant. Reactive black and red dyes were used and the membrane rejection was up to 92-94 % of the two dyes were achieved respectively, while COD removal was up to 94 % in cross-flow cell (Das Gupta *et al.*²²).

De *et al.*, studied unstirred batch and cross flow Nanofiltration with MWCO = 400 Dalton to separate dye from aqueous solutions. Using the experimental results, and model parameters (i.e. the diffusivity of the solute (D) and real retention (R_r)) of the membrane were evaluated by optimizing the experimental flux and permeate concentration profiles (De *et al.*²³). Chaudhari *et al.*, investigated the color removal of commercially azo dyes under anaerobic conditions in wastewater. Color removal was achieved up to 99 % in both the dye containing reactors, whereas COD removals were up to 95 %, 92 % 94 % in control, orange and black dye containing reactors, respectively (Chaudhari *et al.*²⁴).

Woei-Jye & Ismail²⁵, studied the performances of some commercial NF membranes and examined dye rejection, permeate flux and COD rejection as well as studying the transport mechanisms in NF membrane with a brief review of transport models of NF membranes. Jahangiri & Aminian²⁶, compare experimental results with neural network simulation in rejection estimation for two different nanofiltration membranes (NF-90 and DK-5). Arlindo & Isolina²⁷, studied the influence of osmotic pressure and solute adsorption on permeate flux during nanofiltration (NF) in dye wastewater treatment. He also predicts the rejection coefficient using the solution-diffusion model (Tahri *et al.*²⁸).

2. Methodology

The adopted methodology to come up with the performance indicators of applying nanofiltration membranes for dye wastewater is as follows:

- Collection and compiling of nanofiltration (NF) current practice in dye wastewater treatment.
- Determination of the governing process parameters.
- A mathematical correlation through multivariate regression to estimate the performance of using NF membrane in dye wastewater treatment.
- Validation of the regression model using published cases.

3. Results and Discussion

NF data for dye wastewater treatment have been reviewed and analyzed according to technical characteristics. Different data have been collected and excluded due to lack of total information needed regarding reactive dye separation using nanofiltration membranes. Table (1), presents compiled data regarding NF separation systems. The collected data have been refined to determine the parameters governing the separation process. Membranes used in determining this approach are NF90, NF 270, NF 200, SR90, DK2540F and 40-40 TS80 TSF. Multiple regression method is used to predict nanofiltration dye rejection and COD in the permeate values. The correlation developed are based on published data (Arlindo *et al.*²⁷; Chia-Hung *et al.*⁵; Hassani *et al.*²⁹; Woei-Jye & Ismail²⁵; Tahri *et al.*²⁸; Najmeh *et al.*²; Jahangiri & Aminian²⁶; Ahmed *et al.*⁶)

assessed and assembled to formulate the regression model. Eight parameters were selected and investigated, six are considered as independent variables of the multivariate analysis, and two dependent variables. The independent variables are membrane flux, pH, dye rejection, trans-membrane pressure, membrane pore size, COD (in feed and permeate). Tables (2) and (3) shows selected compiled data used for model formulation, showing a strong relationship between the investigated variables and the estimated values.

The final forms of the formulated correlation are mentioned below in equation (1) and (2)

$$\text{Dye Rejection (\%)} = (-880.248) + (104.552 * \text{Cond}) + (-25 * \text{Flux}) + (914.11 * \text{Pore size}) + (-56.218 * \text{pH}) + (24.686 * \text{COD feed}) \dots\dots\dots (1)$$

$$\text{COD rejection} = 82655.46 + (5618.55 * \text{pH}) + (-912 * \text{Feed Conductivity}) + (154.8 * \text{Flux}) + (-404.63 * \text{Pore size}) + (-21.12 * \text{Feed COD}) + (-10.08 * \text{Dye rejection}) \dots\dots(2)$$

Where:

Cond.= Feed conductivity ((ms/cm))/10, Flux = Flux (l/m²h)/10, Pressure = Pressure (bar) /10, COD feed = COD feed/100, Pore size = Pore size (Da)/200

Table (1) Different NF membrane types characteristics for dye wastewater treatment

| Dye type | NF membrane Type | pH | Feed water conductivity (ms/cm) | Flux (l/m ² h) | Transmembrane Pressure (bar) | Membrane pore size (Da) | COD in | COD out | Dye rejection | Ref |
|--------------|------------------|------|---------------------------------|---------------------------|------------------------------|-------------------------|--------|---------|---------------|------|
| reactive dye | DK2540F | 10.6 | 17 | 49 | 12 | 200 | 2450 | 612 | 98 | [30] |
| reactive dye | DK2540F | 9.2 | 14 | 40.5 | 12 | 200 | 2160 | 324 | 95 | [30] |
| reactive dye | NF200 | 7.1 | 6 | 1.5 | 15 | 250 | 708 | 212 | 97 | [31] |
| reactive dye | NF270 | 7.1 | 6 | 1.1 | 15 | 250 | 708 | 140 | 98 | [31] |
| reactive dye | SR90 | 7.1 | 10 | 50 | 14 | 250 | 890 | 700 | 50 | [32] |
| reactive dye | NF90 | 7.1 | 10 | 50 | 14 | 250 | 890 | 448 | 75 | [32] |
| reactive dye | 40-40 TS80 TSF | 6.5 | 42 | 9 | 5 | 200 | 20 | 9 | 90 | [33] |

Table (2) Coefficient of determination (R^2) and the error
(Chia-Hung *et al.*⁵; Hassani *et al.*²⁹; Tahri *et al.*²⁸; Ahmed *et al.*⁶)**Probability (P-value), Summary output for Dye Rejection estimate using NF**

| <i>Regression Statistics</i> | | | | |
|------------------------------|---------------------|-----------------------|---------------|----------------|
| Multiple R | 0.91514 | | | |
| R Square | 0.857481 | | | |
| Adjusted R Square | -0.97511 | | | |
| Standard Error | 17.67767 | | | |
| Observations | 7 | | | |
| ANOVA | | | | |
| | <i>df</i> | <i>SS</i> | <i>MS</i> | <i>F</i> |
| Regression | 6 | 1610.357 | 268.3929 | 1.030629 |
| Residual | 1 | 312.5 | 312.5 | |
| Total | 7 | 1922.857 | | |
| | <i>Coefficients</i> | <i>Standard Error</i> | <i>t Stat</i> | <i>P-value</i> |
| Intercept | -880.248 | 34379.25 | -0.0256 | 0.983704 |
| pH | -56.2185 | 2188.507 | -0.02569 | 0.98365 |
| Feed Conductivity | 104.5524 | 3720.019 | 0.028105 | 0.982112 |
| Flux | -25 | 625 | -0.04 | 0.974549 |
| Pressure | 0 | 0 | 65535 | |
| Pore size | 914.1117 | 33370.39 | 0.027393 | |
| COD feed | 24.68629 | 854.8369 | 0.028878 | 0.981621 |

The results showed that the rejection of reactive dyes by NF membranes highly dependent on the variation in the salt content of the feed stream and the membrane type (pore size) and independent on the applied pressure. These results are compatible with the published results of (Chollom *et al.*³⁴). Salt rejections and permeate flux rates are dependent on feed pressure, however, for the studied range; no influence was noticed on the studied variables.

Table (3) Coefficient of determination (R^2) and the error probability (P-value), Summary output for COD value estimate in permeate by using NF

| <i>Regression Statistics</i> | | | |
|------------------------------|---------------------|-----------------------|---------------|
| Multiple R | 1 | | |
| R Square | 1 | | |
| Adjusted R Square | 65535 | | |
| Standard Error | 0 | | |
| Observations | 7 | | |
| ANOVA | | | |
| | <i>df</i> | <i>SS</i> | <i>MS</i> |
| Regression | 8 | 380845.4286 | 47605.67857 |
| Residual | 0 | 0 | 65535 |
| Total | 8 | 380845.4286 | |
| | | | |
| | <i>Coefficients</i> | <i>Standard Error</i> | <i>t Stat</i> |
| Intercept | 82655.45788 | 0 | 65535 |
| - | 0 | 0 | 65535 |
| pH | 5618.553443 | 0 | 65535 |
| Conductivity | -9120.01731 | 0 | 65535 |
| Flux | 1548 | 0 | 65535 |
| Pressure | 0 | 0 | 65535 |
| Pore size | -80926.39431 | 0 | 65535 |
| COD feed | -2112.941251 | 0 | 65535 |
| Membrane Rejection | -10.08 | 0 | 65535 |

Figure (1), shows the deviation percent between estimated values and published case studies/data (Nur et al.³⁵; Arlindo et al.²⁷; Chia-Hung et al.⁵; Hassani et al.²⁹; Mehmet et al.³⁶; Woei-Jye²⁵; Tahri et al.²⁸; Aouni et al.³⁰; Najmeh et al.²; Jahangiri & Aminian²⁶; Chollom et al.³⁴; Reza et al.³²; Najmeh et al.³³, and Ahmed et al.⁶). The values show that the percent deviation for COD value estimation is almost neglected, while for rejection estimation of about 15%.

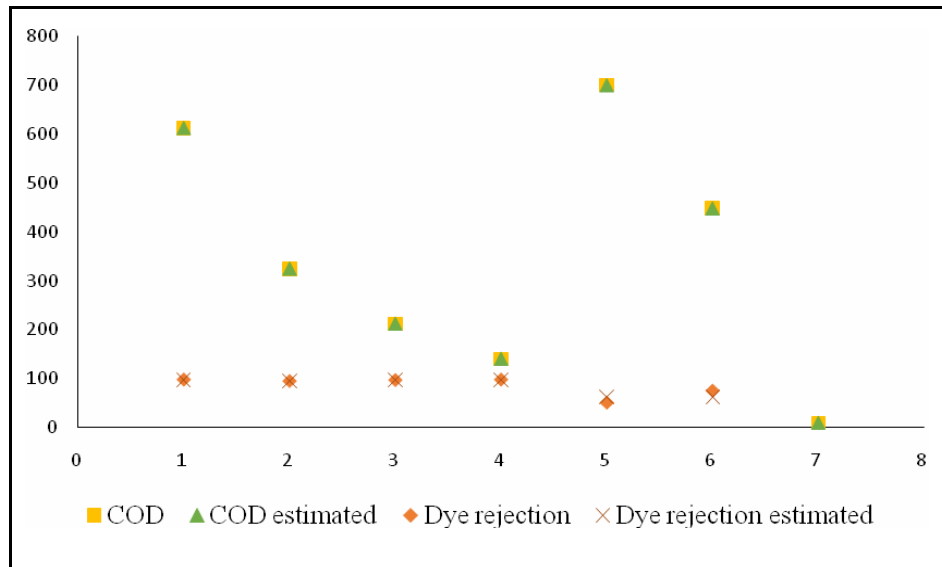


Figure (1) Comparison between estimated and published values

4. Conclusion

Due to the environmental concerns regarding treatment and recycling of dye wastewater. Nanofiltration present a reliable option for dye wastewater treatment and presenting an option of water recycling. Multivariate regression models have been developed to predict membrane performance regarding reactive dyes rejection as well as COD concentration in the permeate stream. Eight parameters have been selected and investigated, six of them set were as the independent variables of the multivariate analysis and two dependent variables. Validation of the presented models by comparing the results with published data to give a reliable estimation on COD and rejection values of the membrane used under the pre-mentioned parameters.

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