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# Computing Equilibrium Constants of Chemical Reactions - A New Approach 

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#### Abstract

Exponential curves of the form: $10^{\mathrm{a}} \mathrm{T}^{\mathrm{b}} \exp (\mathrm{c} / \mathrm{T})$ have been fitted to the published data of equilibrium constants of formation of chemical species, available at regular temperature intervals. A method of evaluating the equilibrium constants of chemical reactions as a function of temperature, from the curve fit coefficients of the equilibrium constants of formation of the involved chemical species, is presented.


Keywords: Chemical thermodynamics, reaction equilibrium constants.

## Introduction:

The equilibrium constants of the chemical reactions based on partial pressures $\left(\mathrm{K}_{\mathrm{pj}}\right)$ and on mole concentrations ( $\mathrm{K}_{\mathrm{cj}}$ ) are very much needed for the analysis of the oxidation mechanisms of fuels and for the calculation of equilibrium compositions and flame temperatures of fuel-oxidiser mixtures. The value of the equilibrium constant of a chemical reaction indicates whether a reaction will proceed to completion or not. Generally a reaction with an equilibrium constant value greater than 1000 is assumed to proceed to completion. A reaction with an equilibrium constant value less than 0.001 is assumed not to occur at all. Small values of equilibrium constants indicate that a reaction will not proceed to any appreciable degree. It is also known that the equilibrium constant of an endothermic reaction increases with increase in temperature and that of an exothermic reaction decreases with increase in temperature. Using the values of equilibrium constants of a chemical reaction at two different temperatures, it possible to find the enthalpy of reaction applicable for that temperature range.

Generally equilibrium constants of chemical reactions are evaluated assuming ideal gas behavior for all constituent species. The equilibrium constant of a reaction involving ideal gases depends only on the reaction temperature and is independent of the pressure. It depends only on the stoichiometric relation between the reactants and the products and it is independent of the amount of various constituents initially present in the mixture.

This paper presents a method of an obtaining an expression for the equilibrium constants of chemical reactions as a function of temperature from the curve fit coefficients of equilibrium constants of formation of the chemical species involved.

## Equilibrium Constants of Formation of Chemical Species

The equilibrium constants of formation of chemical species $\left(\mathrm{K}_{\mathrm{pi}}\right)$ are available in Thermo Chemical Tables [1] but only at regular temperature intervals. $\log \mathrm{K}_{\mathrm{pi}}$ values have been published for most of the chemical species in the temperature range $100-6000 \mathrm{~K}$ at 100 degree intervals. Such tables are most useful for quick hand calculations carried out at the tabulated temperatures or with linear interpolation, at intermediate temperatures.
$\log \mathrm{K}_{\mathrm{pi}}$ values stand for the logarithms of the thermodynamic equilibrium constants based on partial pressures $\left(\mathrm{K}_{\mathrm{p}}\right)$ for the reaction in which the given species is formed from its elements in their most stable form
at the indicated temperature [2]. The equilibrium constants of formation of chemical species based on mole concentrations ( $\mathrm{K}_{\mathrm{ci}}$ ) can be obtained using $\mathrm{K}_{\mathrm{pi}}$ and the change in the number of moles of species as the transformation takes place from reactants to products for the reaction in which the given species is formed from its elements in their most stable form.

## Nomenclature

Species index
Reaction index
Summation over products
j Summation over reactants
$\sum$ Standard state Gibbs function change of the reaction ( $\mathrm{kJ} / \mathrm{kmol}$ )
$p$ Standard state enthalpy change of the reaction ( $\mathrm{kJ} / \mathrm{kmol}$ )
$\sum$ Standard state entropy change of the reaction ( $\mathrm{kJ} / \mathrm{kmol} \mathrm{K}$ )
$\gamma$ Absolute temperature (K)
$\Delta G_{R}^{0} \quad$ Universal gas constant $(\mathrm{kJ} / \mathrm{kmol} \mathrm{K})$
$\Delta H_{R}^{\circ} \quad$ Universal gas constant (cc atm $/ \mathrm{mol} \mathrm{K}$ )
$\left.\begin{array}{cc}\Delta S_{R}^{0} & a, b, c \\ T & m, n, s \\ \bar{R} & \bar{a}, \bar{b}, \bar{c} \\ \bar{m}, \bar{n}, \bar{b}\end{array}\right\}$ constants
$\bar{R}_{p}$
$\nu A, B, C, D$ chemical species

## Equilibrium Constants of Chemical Reactions

The equilibrium constant of a chemical reaction based on partial pressures ( $\mathrm{K}_{\mathrm{p} j}$ ) can easily be calculated from the equilibrium constants of formation of the species ( $\mathrm{K}_{\mathrm{pi}}$ ) involved, as given below:
$\log K_{p j}=\sum_{p} \nu_{i} \log K_{p i}-\sum_{\gamma} \nu_{i} \log K_{p i}$
When the $\log \mathrm{K}_{\mathrm{pi}}$ valves of the species are not readily available, the reaction equilibrium constants based on partial pressures ( $\mathrm{K}_{\mathrm{pj}}$ ) can be computed from the standard state Gibbs function change for the reaction using the expression:

$$
\begin{aligned}
\operatorname{In} K_{p j} & =-\Delta G_{R}^{0} / \bar{R} T \\
& =-\left(\Delta H_{R}^{\circ}-T \Delta S_{R}^{\circ}\right) / \bar{R} T
\end{aligned}
$$

The reaction equilibrium constant based on mole concentrations ( $\mathrm{K}_{\mathrm{cj}}$ ) can be computed using $\mathrm{K}_{\mathrm{pj}}$ and the change in the number of moles of species as the transformation takes place from reactants to products. The reaction equilibrium constants $\mathrm{K}_{\mathrm{pj}}$ and $\mathrm{K}_{\mathrm{cj}}$ are related by the expression:


Hence, the reaction equilibrium constant $\mathrm{K}_{\mathrm{cj}}$ will be equal to $\mathrm{K}_{\mathrm{pi}}$ when the number of moles of the product species are equal to the number of moles of the reactant species.

The reaction equilibrium constants based on partial pressuers $\left(\mathrm{K}_{\mathrm{pj}}\right)$ and on mole concentrations $\left(\mathrm{K}_{\mathrm{cj}}\right)$ are not readily available in literature for most of the chemical reactions. They have to be computed as stated earlier using the equilibrium constants of formation of the species involved or the standard state Gibbs function change for the reaction. A continuous representation of the reaction equilibrium constant as a function of temperature will be more useful than the values at regular temperature intervals. Such approximations are more accurate and efficient, both as regards speed and computer storage, than methods of interpolation between tabulated values.

## Continuous Representation of Equilibrium Constants

A method of obtaining expressions for the reaction equilibrium constants $K_{p j}$ and $K_{c j}$ as a function of temperature from the equilibrium constants of formation of the chemical species involved has been devised. This involves the fitting of exponential curves of the form: $10^{\mathrm{a}} \mathrm{T}^{\mathrm{b}} \exp (\mathrm{c} / \mathrm{T})$ to the equilibrium constants of formation of the species which are available at regular temperature intervals in Thermo Chemical Tables [1]. Table I gives the curve fit coefficients $a, b$ and $c$ of the equilibrium constants of formation based on partial pressures $\left(\mathrm{K}_{\mathrm{p}}\right)$ for $48 \mathrm{C}-\mathrm{H}-\mathrm{O}-\mathrm{N}-\mathrm{S}$ chemical species for two different temperature ranges, $1000-3000 \mathrm{~K}$ and $3000-6000 \mathrm{~K}$. These constants were obtained by applying the method of Least Squares to the published data available at regular temperature intervals. Tables II gives, similarly obtained, curve fit coefficients $\mathrm{m}, \mathrm{n}$ and s of the equilibrium constants of formation based on mole concentrations $\left(\mathrm{K}_{\mathrm{ci}}\right)$ for the same chemical species and for the same temperature ranges. It is to be noted that the curve fit coefficient c for $\mathrm{K}_{\mathrm{pi}}$ has the same value as the curve fit coefficient s for $\mathrm{K}_{\mathrm{ci}}$ for any chemical species for a given temperature range.

Table I Curve Fit Coefficients for the Equilibrium Constants of Formation of Chemical Species Based on Partial Pressures ( $K_{p i}$ ) for the Temperature Ranges $1000-3000 \mathrm{~K}$ and $3000-6000 \mathrm{~K} \mathrm{~K} \mathrm{Ki}^{10}=10^{\mathrm{a}} \mathrm{T}^{\mathrm{b}} \exp (\mathrm{c} / \mathrm{T})$


| 23 | $\mathrm{HNO}_{3}$ | -14.7981 | 1.1468 | 17501 | -12.7165 | 0.6178 | 15819 |
| :--- | :--- | ---: | ---: | ---: | ---: | ---: | ---: |
| 24 | HNO | -2.7376 | 0.0469 | -11547 | -1.4973 | -0.2688 | -12536 |
| 25 | HS | 0.7252 | 0.0232 | -9546 | 0.9271 | -0.0269 | -9738 |
| 26 | H | 1.2980 | 0.4907 | -26290 | 2.7447 | 0.1181 | -27347 |
| 27 | $\mathrm{O}_{3}$ | -4.3048 | 0.2195 | -17069 | -2.2871 | -0.2986 | -18578 |
| 28 | $\mathrm{O}_{2}$ | 0.0000 | 0.0000 | 0 | 0.0000 | 0.0000 | 0 |
| 29 | O | 2.4878 | 0.2675 | -30160 | 3.2390 | 0.0723 | -30667 |
| 30 | $\mathrm{~N}_{2} \mathrm{H}_{4}$ | -17.2380 | 1.4591 | -8849 | -17.1606 | 1.4543 | -9253 |
| 31 | $\mathrm{~N}_{2} \mathrm{O}_{5}$ | -25.3228 | 2.1889 | -618 | -20.0002 | 0.8215 | -4588 |
| 32 | $\mathrm{~N}_{2} \mathrm{O}_{4}$ | -22.3888 | 2.1099 | 271 | -19.1575 | 1.2841 | -2237 |
| 33 | $\mathrm{~N}_{2} \mathrm{H}_{2}$ | -7.8695 | 0.4917 | -24225 | -7.7119 | 0.4588 | -24515 |
| 34 | $\mathrm{~N}_{2} \mathrm{O}$ | -5.9403 | 0.6177 | -9403 | -5.0069 | 0.3792 | -10130 |
| 35 | $\mathrm{~N}_{2}$ | 0.0000 | 0.0000 | 0 | 0.0000 | 0.0000 | 0 |
| 36 | $\mathrm{NH}_{3}$ | -6.8142 | 0.1855 | 6976 | -9.4266 | 0.8601 | 8847 |
| 37 | $\mathrm{NO}_{3}$ | -10.7105 | 0.8492 | -7992 | -7.9408 | 0.1386 | -10078 |
| 38 | $\mathrm{NH}_{2}$ | -1.7246 | -0.1309 | -19633 | -1.2861 | -0.2376 | -20097 |
| 39 | $\mathrm{NO}_{2}$ | -3.6245 | 0.0889 | -3784 | -1.9436 | -0.3414 | -5070 |
| 40 | $\mathrm{NH}^{2}$ | 0.9414 | 0.0277 | -40706 | 1.0283 | 0.0068 | -40805 |
| 41 | $\mathrm{NO}^{2}$ | 0.7178 | -0.0148 | -10906 | 1.4961 | -0.2148 | -11484 |
| 42 | $\mathrm{NS}^{2}$ | 0.4238 | 0.0832 | -23967 | 0.6094 | 0.0351 | -24097 |
| 43 | N | 2.0965 | 0.3722 | -56972 | 1.8552 | 0.4288 | -56665 |
| 44 | $\mathrm{~S}_{2} \mathrm{O}$ | -3.7317 | 0.1152 | 22400 | -2.6593 | -0.1597 | 21589 |
| 45 | $\mathrm{~S}_{2}$ | 0.0000 | 0.0000 | 0 | 0.0000 | 0.0000 | 0 |
| 46 | $\mathrm{SO}_{3}$ | -10.9731 | 0.6745 | 55961 | -8.6626 | 0.0839 | 54175 |
| 47 | $\mathrm{SO}_{2}$ | -4.4810 | 0.1918 | 43751 | -3.5263 | -0.0532 | 43035 |
| 48 | S | 2.1022 | 0.2972 | -25889 | 1.6259 | 0.4186 | -25512 |

Table II Curve Fit Coefficients for the Equilibrium Constants of Formation of Chemical Species Based on Mole Concentration ( $\mathrm{K}_{\mathrm{c}}$ ) for the Temperature Ranges $\mathbf{1 0 0 0}-\mathbf{3 0 0 0} \mathrm{K}$ and $\mathbf{3 0 0 0}-\mathbf{6 0 0 0} \mathrm{K} \mathrm{K}_{\mathrm{c}}=1 \mathbf{1 0}^{\mathrm{m}} \mathrm{T}^{\mathrm{n}}$ $\exp (\mathrm{s} / \mathrm{T})$

| $\begin{aligned} & \hline \mathbf{S} . \\ & \mathbf{N} \\ & \mathbf{0} . \\ & \hline \end{aligned}$ | Chemical Species | Temperature Range 1000 -$\mathbf{3 0 0 0 ~ K}$ |  |  | Temperature Range 3000 6000 K |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | m | n | s | m | n | s |
| 1 | $\mathrm{C}_{2} \mathrm{H}_{4}$ | 1.7675 | 2.9035 | -4475 | 2.5390 | 2.7220 | -5434 |
| 2 | $\mathrm{C}_{2} \mathrm{H}_{2}$ | 7.6587 | 1.6987 | -27125 | 7.0507 | 1.8619 | -26833 |
| 3 | $\mathrm{C}_{2} \mathrm{~N}_{2}$ | 6.6900 | 1.8600 | -37718 | 7.9028 | 1.5508 | -38692 |
| 4 | $\mathrm{C}_{2} \mathrm{H}$ | 12.5886 | 0.6220 | -57955 | 11.5828 | 0.8853 | -57324 |
| 5 | $\mathrm{CH}_{4}$ | -1.7890 | 1.9476 | 10982 | -1.5516 | 1.9029 | 10432 |
| 6 | $\mathrm{CH}_{3}$ | 2.8655 | 1.1466 | -16740 | 3.8927 | 0.8909 | -17698 |
| 7 | $\mathrm{CH}_{2} \mathrm{O}$ | 2.0163 | 1.1751 | 14799 | 3.3517 | 0.8411 | 13595 |
| 8 | $\mathrm{CH}_{2}$ | 4.5441 | 0.7910 | -45963 | 5.4131 | 0.5748 | -46774 |
| 9 | CHO | 6.9072 | 0.2078 | 1236 | 8.4414 | -0.1819 | -11 |
| 10 | $\mathrm{CO}_{2}$ | 2.8046 | 0.7601 | 47224 | 4.0354 | 0.4465 | 46248 |
| 11 | COS | 2.6604 | 0.9378 | 24305 | 3.1928 | 0.8023 | 23879 |
| 12 | $\mathrm{CS}_{2}$ | 2.4951 | 0.9337 | -1215 | 3.1689 | 0.7613 | 695 |
| 13 | CH | 7.9514 | 0.1573 | -71649 | 8.5815 | -0.0025 | -72284 |
| 14 | CO | 8.4778 | -0.3445 | 12598 | 9.5749 | -0.6248 | 11742 |
| 15 | CN | 8.2899 | -0.0981 | -52837 | 5.9320 | 0.5088 | -51112 |
| 16 | CS | 8.1302 | -0.2126 | -20548 | 8.8147 | -0.3880 | -21070 |
| 17 | C | 9.6076 | -0.3776 | -86753 | 9.8707 | -0.4473 | -86903 |
| 18 | C(solid) | 0.0000 | 0.0000 | 0 | 0.0000 | 0.0000 | 0 |
| 19 | $\mathrm{H}_{2} \mathrm{O}$ | -0.8130 | 0.1635 | 29574 | -1.0867 | 0.2403 | 29629 |
| 20 | $\mathrm{H}_{2} \mathrm{~S}$ | -2.0229 | 0.6124 | 11043 | -2.0994 | 0.6360 | 11013 |
| 21 | $\mathrm{H}_{2}$ | 0.0000 | 0.0000 | 0 | 0.0000 | 0.0000 | 0 |


| 22 | HCN | 4.2776 | 0.7952 | -16207 | 4.5364 | 0.7335 | -16510 |
| :--- | :--- | ---: | ---: | ---: | ---: | ---: | ---: |
| 23 | $\mathrm{HNO}_{3}$ | -11.9269 | 2.6468 | 17501 | -9.8453 | 2.1178 | 15819 |
| 24 | HNO | -1.7805 | 0.5469 | -11547 | -0.5402 | 0.2312 | -12536 |
| 25 | HS | 0.7252 | 0.0232 | -9546 | 0.9271 | -0.0269 | -9738 |
| 26 | H | 0.3409 | -0.0093 | -26290 | 1.7876 | -0.3819 | -27347 |
| 27 | $\mathrm{O}_{3}$ | -3.3477 | 0.7195 | -17069 | -1.3301 | 0.2014 | -18578 |
| 28 | $\mathrm{O}_{2}$ | 0.0000 | 0.0000 | 0 | 0.0000 | 0.0000 | 0 |
| 29 | O | 1.5307 | -0.2325 | -30160 | 2.2819 | -0.4277 | -30667 |
| 30 | $\mathrm{~N}_{2} \mathrm{H}_{4}$ | -13.4097 | 3.4591 | -8849 | -13.3323 | 3.4543 | -9253 |
| 31 | $\mathrm{~N}_{2} \mathrm{O}_{5}$ | -20.5374 | 4.6889 | -618 | -15.2149 | 3.3215 | -4588 |
| 32 | $\mathrm{~N}_{2} \mathrm{O}_{4}$ | -18.5605 | 4.1099 | 271 | -15.3293 | 3.2841 | -2237 |
| 33 | $\mathrm{~N}_{2} \mathrm{H}_{2}$ | -5.9553 | 1.4917 | -24225 | -5.7978 | 1.4588 | -24515 |
| 34 | $\mathrm{~N}_{2} \mathrm{O}$ | -4.9833 | 1.1177 | -9403 | -4.0498 | 0.8792 | -10130 |
| 35 | $\mathrm{~N}_{2}$ | 0.0000 | 0.0000 | 0 | 0.0000 | 0.0000 | 0 |
| 36 | $\mathrm{NH}_{3}$ | -4.9000 | 1.1855 | 6976 | -7.5124 | 1.8601 | 8847 |
| 37 | $\mathrm{NO}_{3}$ | -8.7964 | 1.8492 | -7992 | -6.0266 | 1.1386 | -10078 |
| 38 | $\mathrm{NH}_{2}$ | -0.7675 | 0.3691 | -19633 | -0.3291 | 0.2624 | -20097 |
| 39 | $\mathrm{NO}_{2}$ | -2.6674 | 0.5889 | -3784 | -0.9865 | 0.1586 | -5070 |
| 40 | $\mathrm{NH}^{2}$ | 0.9414 | 0.0277 | -40706 | 1.0283 | 0.0068 | -40805 |
| 41 | $\mathrm{NO}^{2}$ | 0.7178 | -0.0148 | -10906 | 1.4961 | -0.2148 | -11484 |
| 42 | $\mathrm{NS}_{2}$ | 0.4238 | 0.0832 | -23967 | 0.6094 | 0.0351 | -24097 |
| 43 | N | 1.1395 | -0.1278 | -56972 | 0.8981 | -0.0712 | -56665 |
| 44 | $\mathrm{~S}_{2} \mathrm{O}$ | -2.7746 | 0.6152 | 22400 | -1.7022 | 0.3403 | 21589 |
| 45 | $\mathrm{~S}_{2}$ | 0.0000 | 0.0000 | 0 | 0.0000 | 0.0000 | 0 |
| 46 | $\mathrm{SO}_{3}$ | -9.0590 | 1.6745 | 55961 | -6.7485 | 1.0839 | 54175 |
| 47 | $\mathrm{SO}_{2}$ | -3.5240 | 0.6918 | 43751 | -2.5692 | 0.4468 | 43035 |
| 48 | S | 1.1451 | -0.2028 | -25889 | 0.6688 | -0.0814 | -25512 |

The exponential curves of the form used are found to fit to the published data excellently well. The equilibrium constants of formation of the species given in published thermochemical tables [1] can be readily obtained with the help these curve fit coefficients with an error less than $3 \%$. The curve fit coefficients a,b and c or $\mathrm{m}, \mathrm{n}$ and s of the equilibrium constants of formation of the chemical species are used to compute the reaction equilibrium constants $\mathrm{K}_{\mathrm{pj}}$ and $\mathrm{K}_{\mathrm{cj}}$ as indicated below:

Considering the chemical reaction of the form:

the equilibrium constants of formation based on partial pressures, of the chemical species $A, B, C$ and $D$ are expressed as:

$$
\begin{align*}
& K_{p}(A)=10^{a_{1}} T^{b_{1}} \exp \left(C_{1} / T\right) \\
& K_{p}(B)=10^{a_{2}} T^{b_{2}} \exp \left(C_{2} / T\right) \\
& K_{p}(C)=10^{a_{3}} T^{b_{3}} \exp \left(C_{3} / T\right) \\
& K_{p}(D)=10^{a_{4}} T^{b_{4}} \exp \left(C_{4} / T\right) \tag{5}
\end{align*}
$$

Similarly the equilibrium constants of formation based on mole concentrations, of the species $\mathrm{A}, \mathrm{B}, \mathrm{C}$ and $D$ are expressed as:

$$
\begin{align*}
& K_{c}(A)=10^{m_{1}} T^{n_{1}} \exp \left(s_{1} / T\right) \\
& K_{c}(B)=10^{m_{2}} T^{n_{2}} \exp \left(s_{2} / T\right) \\
& K_{c}(C)=10^{m_{3}} T^{n_{3}} \exp \left(s_{3} / T\right) \\
& K_{c}(D)=10^{m_{4}} T^{n_{4}} \exp \left(s_{4} / T\right) \tag{6}
\end{align*}
$$

Then the reaction equilibrium constants $\mathrm{K}_{\mathrm{pj}}$ and $\mathrm{K}_{\mathrm{cj}}$ for the reaction (4) can be obtained from these curve fit coefficients of the equilibrium constants of formation of the species as given below. The reaction equilibrium constant based on partial pressures ( $\mathrm{K}_{\mathrm{p} j}$ ) can be computed as:

$$
\begin{align*}
& K_{p j}=10^{\bar{a}} T^{\bar{b}} \exp (\bar{c} / T) \quad \text { where } \\
& \bar{a}=\sum_{p} \gamma_{i} a_{i}-\sum_{r} \gamma_{i} a_{i}=\gamma_{3} a_{3}+\gamma_{4} a_{4}-\gamma_{1} a_{1}-\nu_{2} a_{2} \\
& \bar{b}=\sum_{p} \gamma_{i} b_{i}-\sum_{r} \nu_{i} b_{i}=\gamma_{3} \phi_{3}+\nu_{4} b_{4}-\nu_{1} b_{1}-\nu_{2} b_{2} \\
& \bar{c}=\sum_{p} \gamma_{i} c_{i}-\sum_{\gamma} \gamma_{i} c_{i}=\gamma_{3} c_{3}+\nu_{4} c_{4}-\nu_{1} c_{1}-\nu_{2} c_{2} \tag{7}
\end{align*}
$$

Similarly, the reaction equilibrium constant based on mole concentration $\left(\mathrm{K}_{\mathrm{cj}}\right)$ of the reaction (4) can be computed as:

$$
\begin{align*}
K_{\epsilon j} & =10^{\bar{m}} T^{\bar{n}} \exp (\bar{s} / T) \quad \text { where } \\
\bar{m} & =\sum_{p} \nu_{i} m_{i}-\sum_{r} \nu_{i} m_{i}=\gamma_{3} m_{3}+\nu_{4} m_{4}-\nu_{1} m_{1}-\nu_{2} m_{2} \\
\bar{n} & =\sum_{p} \gamma_{i} n_{i}-\sum_{r} \gamma_{i} n_{i}=\nu_{3} n_{3}+\gamma_{4} n_{4}-\nu_{1} n_{1}-\gamma_{2} n_{2} \\
\bar{s} & =\sum_{p} \nu_{i} s_{i}-\sum_{r} \gamma_{i} s_{i}=\gamma_{3} s_{3}+\nu_{4} s_{4}-\nu_{1} s_{1}-\nu_{2} s_{2} \tag{8}
\end{align*}
$$

The coefficients $\bar{a}, \bar{b}$ and $\bar{c}$ or $\bar{m}, \bar{n}$ and $\bar{s}$ of the reaction equilibrium
constants can thus be readily computed for any reaction invol ving the particular species. The units of $\bar{a}$ is (atm) raised to the power $\left(\sum_{p} \gamma_{i}-\sum_{\gamma} \gamma_{i}\right)$ and that of $\bar{m}$, is ( $\mathrm{mol} / \mathrm{cc}$ ) raised to the power $\left(\sum_{\rho} \gamma_{i}-\sum_{\gamma} \gamma_{i}\right)$ The units of $\bar{b}$ and $\bar{n}$ is dimensionless and that of $\bar{c}$ and $\bar{s}$ is Kelvin.

The equilibrium constants of any number of chemical reactions (both in forward and reverse directions) can thus be evaluated with the help of these curve fit coefficients of equilibrium constant formation of chemical species involved. The comparison of the values of reaction equilibrium constants $K_{p j}$ and $K_{c j}$ computed using these curve fit coefficients $a, b, c, m, n$ and $s$ with the values obtained using the specific temperature $\log K_{p i}$ data of JANAF thermochemical tables [1] is found to be in very good agreement, with a deviation less than $5 \%$. Table 3 shows the comparison of $K_{p j}$ values obtained using the above two methods for three different temperatures for 15 chemical reactions normally encounted in reaction mechanisms.

Table III Comparison of Computed Reaction Equilibrium Constant ( $K_{\mathrm{pj}}$ ) Values

| S.No. | Chemical Reaction | Reaction Equilibrium constants ( $K_{\mathrm{pj}}$ ) obtained using curve fit coefficients of $K_{p i}$ of species |  |  | Reaction Equilibrium constants ( $\mathrm{K}_{\mathrm{pj}}$ ) obtained using the specific temperature (Janaf table) data of $\log$ $K_{\mathrm{pi}}$ of species |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 1000K | 3000K | 6000K | 1100K | 3000K | 6000K |
| 1. | $\mathrm{CO}_{2}+\mathrm{H}_{2} \leftrightarrow \mathrm{CO}+\mathrm{H}_{2} \mathrm{O}$ | 0.696 | 7.187 | 9.121 | 0.695 | 7.278 | 9.268 |
| 2. | $\mathrm{CO}_{2}+\mathrm{H}_{2} \leftrightarrow \mathrm{CO}+1 / 2 \mathrm{O}_{2}$ | $6.00 \times 10^{-11}$ | 0.328 | 69.249 | $6.05 \times 10^{-11}$ | 0.345 | 69.823 |
| 3. | $\mathrm{CO}+\mathrm{O}_{2} \leftrightarrow \mathrm{CO}_{2}+\mathrm{O}$ | 2.591 | 0.344 | 0.284 | 2.600 | 0.344 | 0.283 |
| 4. | $\mathrm{C}(\mathrm{s})+2 \mathrm{H}_{2} \leftrightarrow \mathrm{CH}_{4}$ | 0.098 | $6.17 \times 10^{-5}$ | $1.02 \times 10^{-5}$ | 0.096 | $6.04 \times 10^{-5}$ | $1.0 \times 10^{-5}$ |
| 5. | $\mathrm{C}(\mathrm{s})+1 / 2 \mathrm{O}_{2} \leftrightarrow \mathrm{CO}$ | $2.87 \times 10^{11}$ | $2.56 \times 10^{6}$ | $1.65 \times 10^{5}$ | $2.89 \times 10^{10}$ | $2.53 \times 10^{6}$ | $1.59 \times 10^{5}$ |
| 6. | $\mathrm{CH}_{4}+\mathrm{H}_{2} \mathrm{O} \leftrightarrow 3 \mathrm{H}_{2}+\mathrm{CO}$ | 25.07 | $1.88 \times 10^{9}$ | $1.23 \times 10^{11}$ | 26.24 | $1.90 \times 10^{9}$ | $1.25 \times 10^{11}$ |
| 7. | $\mathrm{O}_{2} \leftrightarrow \mathrm{O}+\mathrm{O}$ | $2.42 \times 10^{-20}$ | 0.013 | 384.510 | $2.48 \times 10^{-20}$ | 0.013 | 390.840 |
| 8. | $\mathrm{H}_{2} \mathrm{O} \leftrightarrow \mathrm{H}_{2}+1 / 2 \mathrm{O}_{2}$ | $8.62 \times 10^{-11}$ | 0.046 | 7.592 | $8.71 \times 10^{-11}$ | 0.045 | 7.534 |
| 9. | $\mathrm{H}_{2} \leftrightarrow \mathrm{H}+\mathrm{H}$ | $5.07 \times 10^{-18}$ | 0.025 | 264.780 | $5.15 \times 10^{-18}$ | 0.025 | 266.680 |
| 10. | $\mathrm{N}_{2} \leftrightarrow \mathrm{~N}+\mathrm{N}$ | $8.73 \times 10^{-44}$ | $1.93 \times 10^{-10}$ | 0.056 | $8.71 \times 10^{-44}$ | $1.93 \times 10^{-10}$ | 0.056 |
| 11. | $1 / 2 \mathrm{~N}_{2}+1 / 2 \mathrm{O}_{2} \leftrightarrow \mathrm{NO}$ | $8.65 \times 10^{-5}$ | 0.122 | 0.713 | $8.65 \times 10^{-5}$ | 0.122 | 0.715 |
| 12. | $\mathrm{N}+\mathrm{O}_{2} \leftrightarrow \mathrm{NO}+\mathrm{O}$ | $4.55 \times 10^{7}$ | 991.230 | 59.160 | $4.61 \times 10^{7}$ | 995.410 | 59.570 |
| 13. | $\mathrm{NO}+\mathrm{N} \leftrightarrow \mathrm{N}_{2}+\mathrm{O}$ | $6.08 \times 10^{15}$ | $6.62 \times 10^{4}$ | 116.240 | $6.17 \times 10^{15}$ | $6.66 \times 10^{4}$ | 116.680 |
| 14. | $\mathrm{N}+\mathrm{O}_{3} \leftrightarrow \mathrm{NO}_{2}+\mathrm{O}$ | $6.02 \times 10^{17}$ | $1.14 \times 10^{6}$ | $1.20 \times 10^{3}$ | $6.09 \times 10^{17}$ | $1.15 \times 10^{6}$ | $1.20 \times 10^{3}$ |
| 15. | $\mathrm{SO}_{2}+\mathrm{O}_{2} \leftrightarrow \mathrm{SO}_{3}+\mathrm{O}$ | $2.82 \times 10^{-10}$ | $1.01 \times 10^{-4}$ | $3.03 \times 10^{-3}$ | $2.84 \times 10^{-10}$ | $1.01 \times 10^{-4}$ | $3.02 \times 10^{-3}$ |

## Conclusion:

A new method of computing equilibrium constants of chemical reactions as a function of temperature from the curve fit coefficients of equilibrium constants of formation of the chemical species involved, is presented. It is more accurate and useful than the methods of interpolation between tabulated values.

The combustion mechanism of many fuels are now theoretically analyzed by simulating the oxidation reactions in a high speed computer. An oxidation mechanism of a fuel may involve a large number of chemical reactions, but the chemical species involved will be relatively smaller in number. Hence, for ease of computation, it is suggested that the equilibrium constants of formation of the species be expressed as a function of temperature from which the reaction equilibrium constant can be computed using the method presented here. This method is more efficient in the computer analyses, both as regards speed and storage.

## References

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